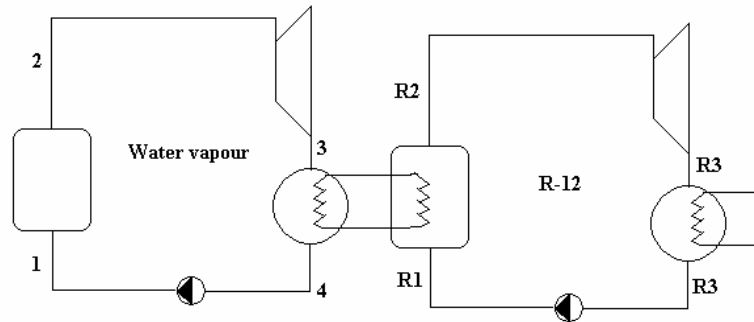


Q1 A steam power plant operates on the Rankine cycle. The high pressure steam is at 60 bar and 500°C at entry to the turbine. The turbine produces 20 MW of power. The condenser pressure is 2 bar.

During day time operation the waste heat from the condenser is used for process heating. During night time operation the waste heat is used in a R-12 power plant that also operates on the Rankine cycle. The refrigerant cycle uses vapour with no superheat at 80°C at entry to the turbine and condenses at 10°C.

Assuming no heat losses and negligible power usage at the pumps, calculate the power output from the R-12 cycle and the thermal efficiency of the plant. The isentropic efficiency of both turbines is 85%. (This question very similar to Q1 1997)

SOLUTION



WATER/VAPOUR CYCLE.

$$h_4 = h_f @ 2 \text{ bar} = 505 \text{ kJ/kg} \quad h_1 = h_4 = 505 \text{ kJ/kg}$$

$$h_2 = h @ 60 \text{ bar and } 500^\circ\text{C} = 3421 \text{ kJ/kg}$$

$$s_2 = s @ 60 \text{ bar and } 500^\circ\text{C} = 6.879 \text{ kJ/kg K}$$

$$s_{3'} = s_2 = 6.879 \text{ kJ/kg K} = s_f + x s_{fg} @ 2 \text{ bar}$$

$$6.879 = 1.530 + 5.597x \quad x = 0.9557$$

$$h_{3'} = h_f + x h_{fg} @ 2 \text{ bar} = 505 + 0.9557 \times 2202 = 2609.4 \text{ kJ/kg}$$

$$\text{Power out} = 20\,000 \text{ kW} = m_s \times \eta_t (3421 - 2609.4)$$

$$20\,000 = m_s \times 0.85 (3421 - 2609.4)$$

$$m_s = 20\,000 / 689.8 = 29 \text{ kg/s}$$

We need to find h_3 . $\frac{3421 - h_3}{3421 - 2609.4} = 0.85 \quad h_3 = 2731 \text{ kJ/kg}$

Check Power out = $29(3421 - 2731) = 20\,000 \text{ kW}$
 Heat lost from the condenser = $29(h_3 - h_4) = 29(2731 - 505) = 64554 \text{ kW}$
 This becomes the heat input to the evaporator in the R-12 cycle.

R-12 CYCLE

$$h_{R2} = h_g @ 80^\circ\text{C} = 212.83 \text{ kJ/kg}$$

$$h_{R1} = h_{R4} = h_f @ 10^\circ\text{C} = 45.37 \text{ kJ/kg}$$

$$\Phi(\text{in}) = 64554 = m_R(212.83 - 45.37) \quad m_R = 385.48 \text{ kg/s}$$

$$s_{R2} = s_g @ 80^\circ\text{C} = 0.6673 \text{ kJ/kg K} = s_{R3} = s_f + x s_{fg} @ 10^\circ\text{C} = 0.1752 + x(0.6921 - 0.1752)$$

$$x = (0.6673 - 0.1752) / 0.5169 = 0.952$$

$$h_{R3} = h_f + x h_{fg} @ 10^\circ\text{C} = 45.37 + 0.952(191.74 - 45.37) = 184.72 \text{ kJ/kg}$$

$$\text{Power output} = m_R (h_{R2} - h_{R3}) = 385.48 (212.83 - 184.72) = 10\,837 \text{ kW}$$

Thermal efficiency $P(\text{out}) / \Phi(\text{in}) = 10\,837 / 64554 = 0.168$ or 16.8%