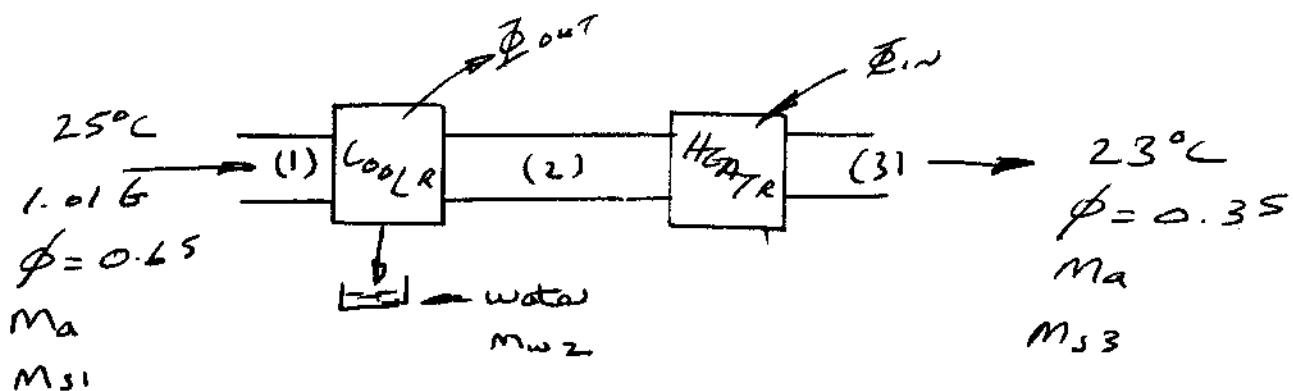


Q8 2002



M_a = MASS OF ^{DRY} AIR - CONSTANT THROUGHOUT
 M_s = MASS OF VAPOUR M_w = MASS OF WATER

$$P_g = 0.03166 \text{ bar} @ 25^\circ\text{C} \quad \rho_s = \phi P_g$$

$$P_{s1} = 0.65 \times 0.03166 = 0.020579 \text{ bar}$$

$$P_a = 1.01 - P_{s1} = 0.989421 \text{ bar}$$

$$\omega_1 = 0.622 \frac{P_{s1}}{P_a} = 0.012937$$

$$M_a = P V / RT = \frac{0.989421 \times 10^5}{287 \times 298} \times V_A$$

$$\text{For } 1 \text{ kg of DRY AIR} \quad V_A = 0.864 \text{ m}^3$$

$$M_{s1} = \frac{P_{s1} V}{R T} \quad \text{FOR VAPOUR VOLUME OF VAPOUR IS SAME AS VOL OF AIR}$$

$$R = 462 \quad \text{FOR WATER VAPOUR}$$

$$M_{s1} = \frac{0.020579 \times 10^5 \times 0.864}{462 \times 298} = 0.012926 \text{ kg}$$

$$\omega = M_s/M_a = 0.622 P_s/P_a$$

$$\phi = P_s/P_g = 1.608 P_a/P_g$$

$$P = 1.01 \text{ bar} \quad \theta = 25^\circ\text{C} \quad \phi = 0.65$$

INLET

$$@ 25^\circ C \quad P_g = 0.03166 \text{ bar}$$

$$\phi = P_s/P_g = 0.65 \quad P_s = 0.65 \times 0.03166 \\ = 0.020579 \text{ bar}$$

$$P_a = 1.01 - 0.020579 = 0.989421 \text{ bar}$$

$$\omega = 0.622 \times \frac{0.020579}{0.989421} = 0.012937$$

Dew Point $\approx 17.8^\circ C$

EXIT

$$\phi_3 = 0.35 = P_{s3}/P_{g3}$$

$$P_{g3} = P_s @ 23^\circ C = 0.02808 \text{ bar}$$

$$P_{s3} = 0.02808 \times 0.35 = 0.009828 \text{ bar}$$

$$P_{a3} = 1.01 - 0.009828 = 1.000172 \text{ bar}$$

$$\omega_3 = 0.622 P_s/P_a = 0.622 \times \frac{0.009828}{1.000172}$$

$$\omega_3 = 0.006111964$$

$$M_{s3} = 0.006112 \text{ Ma}$$

$$M_{s1} = 0.0129206 \text{ Ma}$$

$$\text{CONDENSATE FORMED} = M_{s1} - M_{s3} = 0.00681 \text{ Ma}$$

ENERGY BALANCE ON COOLER

$$P_{s2} = P_{s3} = 0.009828 \text{ bar}$$

$$M_a C_a (\bar{T}_a - \bar{T}_{a2}) - M_w C_w T_w + M_{s1} h_{s1} \\ - M_{s2} h_{s2} = \dot{Q}_{out}$$

$$h_{s1} @ 25^\circ C \quad 0.0206 \text{ bar} = 2550 \text{ kJ/kg (Chart)}$$

$$h_{s2} @ 17.8^\circ C \quad 0.00983 \text{ bar} = h_g = 2533 \text{ kJ/kg}$$

$$M_{a1} = 1 \text{ kg} \quad C_a = 1.004 \text{ kJ/kg K}$$

$$M_{s2} = M_{s3} \quad C_w = 4.186 \text{ kJ/kg K}$$

$$1 \times 1.004 (25 - 17.8) - 0.00681 \times 4.186 \times 17.8$$

$$+ 0.0129206 \times 2550 - 0.006112 \times 2533 = \dot{Q}_{out}$$

$$\dot{Q}_{out} = 24.187 \text{ kJ for 1kg of DRY AIR}$$

ENERGY BALANCE ON HEATER

$$h_{s3} = 2545 \text{ kJ/kg} \quad (23^\circ\text{C} \quad 0.0098286)$$

$$M_a C_a \theta_3 + M_{s3} h_{s3} = M_a C_a \theta_2 + M_{s2} h_{s2} + \dot{Q}(in)$$

$$1 \times 1.004 \times 23 + 0.006112 \times 2545$$

$$= 1 \times 1.004 \times 17.8 + 0.006112 \times 2533 + \dot{Q}(in)$$

$$\dot{Q}(in) = 5.3 \text{ kJ per kg of dry air}$$

$$M_a = 1 \text{ kg at exit} \quad M = M_a + M_{s3}$$

$$M = 1.006112 \text{ kg}$$

$$\begin{aligned} \dot{Q}(out) &= 24.04 \text{ kJ/kg } \\ \dot{Q}(in) &= 5.27 \text{ kJ/kg } \end{aligned} \quad \left. \begin{array}{l} \text{per kg of} \\ \text{conditioned} \\ \text{air} \end{array} \right\}$$