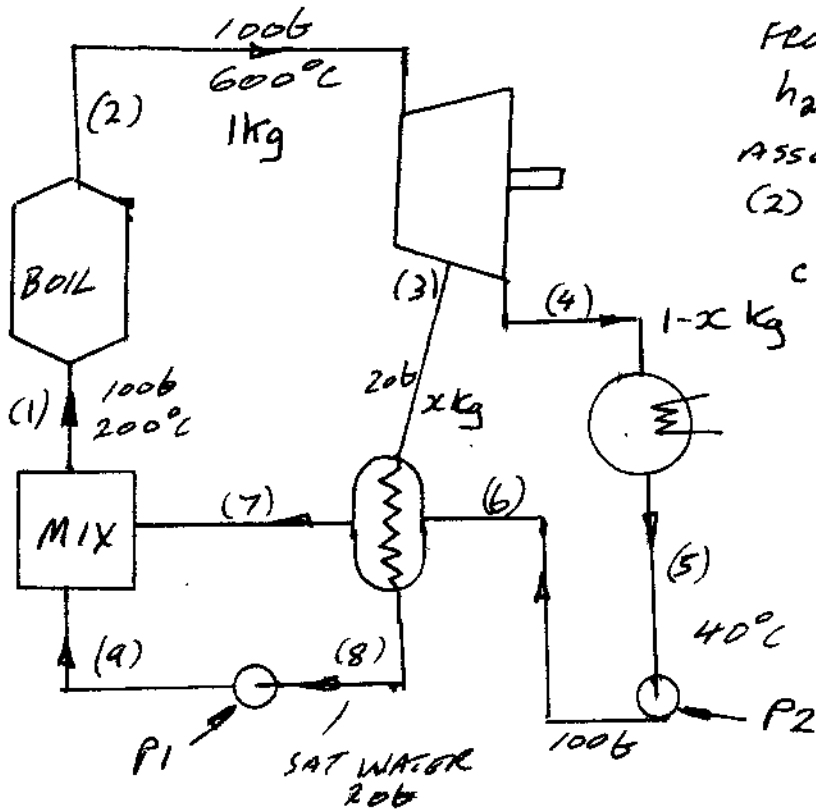
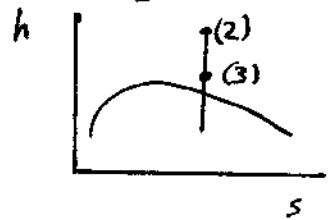


Q5 2001

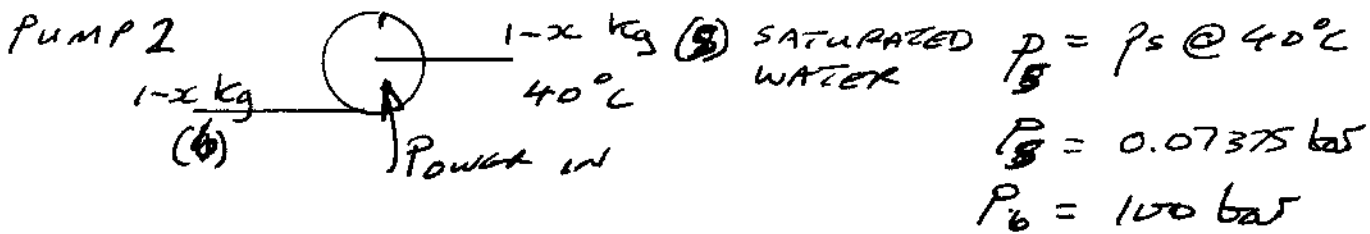


FROM TABLES
 $h_2 = 3624 \text{ kJ/kg}$
 ASSUMING IDEAL EXPANSION
 (2) to (3) FROM
 CHART $h_3 = 3100 \text{ kJ/kg}$



KNOWN POINT AT (1) WATER 100 bar 200°C
 IDEALLY WE NEED WATER TABLES BUT AS
 THEY ARE NOT SUPPLIED $h_1 \approx h_f @ 200^\circ\text{C}$

$$h_1 \approx 855 \text{ kJ/kg}$$



POWER INPUT $\approx \text{Vol} \times \Delta p$ Nominally $v = 0.001 \text{ m}^3/\text{kg}$

$$\text{POWER INPUT} = 0.001 \times (100 - 0.07375) \times 10^5$$

$$= 10000 \text{ J/kg} \text{ or } 10 \text{ kJ/kg}$$

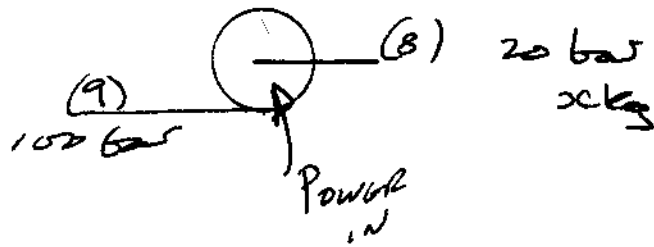
ENERGY BALANCE

$$h_6 = h_5 + 10 \text{ kJ/kg}$$

$$h_5 = h_f @ 40^\circ\text{C} = 167.5 \text{ kJ/kg}$$

$$h_6 = 177.5 \text{ kJ/kg}$$

Pump 1



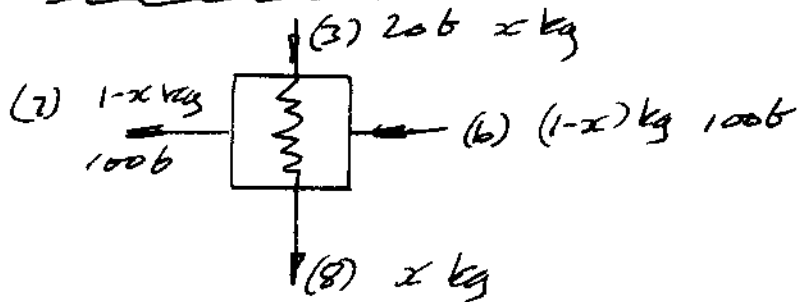
$$\begin{aligned} \text{Power input} &= v \Delta p = 0.001 (100 - 20) \times 10^5 \\ &= 8000 \text{ J/kg} \\ &= 8 \text{ kJ/kg} \end{aligned}$$

ENERGY BALANCE $h_9 = h_8 + 8$

$$h_8 = h_f @ 20 \text{ bar} = 909 \text{ kJ/kg}$$

$$h_9 = 909 + 8 = 917 \text{ kJ/kg}$$

FEED HEATER



$$h_3 = 3100 \text{ kJ/kg}$$

$$h_6 = h_f @ 20 \text{ bar} = 167.5 \text{ kJ/kg}$$

ENERGY BALANCE

$$(1-x) h_6 + x h_3 = (1-x) h_7 + x h_8$$

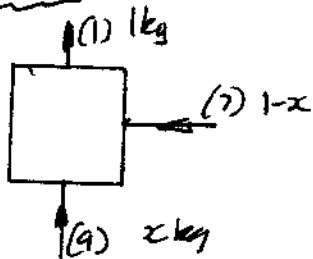
$$(1-x) 177.5 + 3100x = (1-x) h_7 + x (167.5)$$

$$177.5 - 177.5x + 3100x = (1-x) h_7 + 167.5x$$

$$177.5 + 2755x = (1-x) h_7$$

$$h_7 = \frac{177.5 + 2755x}{(1-x)}$$

MIXER



$$1 h_1 = (1-x) h_7 + x h_9$$

$$855 = (1-x) h_7 + x h_9$$

$$855 = (1-x) \left\{ \frac{177.5 + 2755x}{(1-x)} \right\} + 917x$$

$$855 = 177.5 + 2755x + 917x$$

$$677.5 = 3672x \quad x = \underline{\underline{0.184 \text{ kg}}}$$

$$\begin{aligned} \text{Pump 1} \quad P &= 8 \text{ kJ/kg} \\ &= 8 \times 0.184 \text{ kW} \\ &= 1.6 \text{ kW} \end{aligned}$$

$$\begin{aligned} \text{Pump 2} \quad P &= 10 \text{ kJ/kg} \\ &= 10 \times (1 - 0.184) \text{ kW} \\ &= 8.16 \text{ kW} \end{aligned}$$

Based on 1 kg/s Total flow